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Heat Losses

and

Efficiencies

of

Otto Gas Engine.

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Berks
Co., A. H. Smith

Test of a One-Third Horse Power Otto Gas Engine.

The following thesis is an account of a test on a one-third horse power Otto Gas Engine, manufactured by the Otto Gas Engine Company, 33rd and Walnut Streets Philadelphia, to determine the heat distribution, efficiencies and indicated and brake horse powers.

The engine is part of the equipment of the mechanical laboratory of the University of Pennsylvania.

Two half hour-thirty minute-runs were made with the conditions as nearly identical as possible and they were taken together and worked up as one

test.

In the following description, the letters and numbers refer to the photograph of the engine and the apparatus used during the test on page 14a:

The engine consists of a vertical cylinder (16), 3 inches in diameter with a trunk piston packed with 5 metallic rings. The piston [is connected to a cranked shaft (1) by the connecting rod (2)] which has a 5 inch stroke.]

On one end of the shaft is the fly-wheel (10), two feet in diameter, and on the other a gear wheel, which gears into another wheel having twice the number of teeth. These gear wheels are enclosed in the cast iron case (y).

On the shaft of the second gear wheel is an eccentric which operates the rod (22). This in turn operates the exhaust valve (u) and the governor (r). The governor controls the admission of the gas to the chamber (v) where it is stored before being admitted to the cylinder. The gas together with the air is admitted to the cylinder by the disc valve (w) which is raised by suction every fourth stroke of the piston. This valve has a number of holes in its seat which communicate with the chamber (v). Underneath, the valve is in communication with the air space between the bottom wall of the cylinder and the base of

the engine. When the valve is raised a mixture of air and gas is admitted which depends on the relative area through the holes and under the valve. The valve is held to its seat by a spring.

The governor consists of a round, threaded weight (2) on the end of a lever having a screw-thread and a lock nut so the position of the weight can be changed. Its fulcrum is at (q) and the further end of the lever is held down by the spring (o). The pivot at (q) is part of the valve rod (22). Projecting downward from the fulcrum is a small rod (p) which is cast in one piece with the lever and which car-

nes a hook at its lower end. When the rod (p) hangs vertical the hook on the rod engages with a projection on the stem of the valve at (t) being held to its place by the spring (o). When the rod (22) is lifted the governour goes with it and the valve is raised admitting gas to the chamber (V). If the speed gets too fast the inertia of the weight overcomes the pull of the spring and causes the hook to miss the projection. The valve is not raised and no gas admitted. Consequently there is no explosion and the speed is reduced. The speed can be regulated by the position of the weight (r) on the

lever.

The gas is drawn from the main and passes through the meter (d), the equalizing bag (f) and the tap (g). The latter is supplied with a graduated disc and pointer.

The gas for the Bunsen burner enclosed in the cast iron cylinder (h) is drawn through the meter (e) and the regulating cock (23). This cylinder is lined with asbestos and an iron tube of small diameter, closed at the top, extends up the centre. The fire plays round this tube and keeps it red hot. The charge is compressed into this tube and exploded.

The air used is admitted

to the space below the cylinder wall through the pipe (6) and also through small holes in the bedplate.

The exhaust gases pass out through the exhaust valve (m) and the pipes (i) and (18) into the outside air.

A water jacket surrounds the cylinder, the water entering at the bottom and exhausting at the top through pipes at the back which cannot be seen in the picture. By means of pet cocks the water can be exhausted through the floor or discharged into collecting buckets.

The engine works in what is known as an 'Otto Cycle' and takes four strokes to complete a cycle. On the

first upward stroke the mixture is drawn into the cylinder; on the downward it is compressed.

It is exploded as the engine reaches the dead point; on the third expansion the flame and on the fourth, the exhaust.

The suction valve takes care of itself, when it comes to the second gear wheel in the case (y) having twice the number of teeth on the first the other valves are opened every fourth stroke instead of every second.

Several precautions are necessary. All the valves must be kept clean and fit their seats truly or the engine will not run.

If the compression is not

good there will not be any explosion. The valve (w) must also be adjusted so that it is not raised too easily or too much. The supply of gas must also be regulated to suit the load, as for any given load there are certain limits in each direction for the ratio of air to gas and if these limits are passed there is no explosion and the engine stops. The ignition tube must also be kept hot. On starting the flywheel must be spun comparatively fast before an explosion will occur.

Instruments.

The following apparatus was used:

The brake for determining the brake horsepower consisted of a strong cord (8) held in position by three wooden guides (9). On one end is hung a weight while to the other is attached the spring balance (7) which was held by a hook (19) in the floor.

The cards for the indicated horse power were taken with a Tuonon Indicator (3) having a piston with an area of one quarter square inch and a larger one of one half a square inch. It was attached to the pipe (24) in connection with the lower

part of the cylinder. Communication was through a cock (2) on the pipe. The larger cylinder was used.

To get the required motion for the drum (3), a string (12) was fastened to a pin projecting from the hub of the fly wheel. This string was strong and was tied so it would not tighten and wrap up on the pin. It carried a loop at the lower end. Another string (25) was wound around the drum and had a hook on its free end. When the engine was running the string (12) was flung out by centrifugal force and could be caught in the hand. The hook of (25) was then placed in the loop of string (12) and the desired motion given to the drum (3).

For the number of revolutions the counter (m) was fastened to a wooden frame and held firmly by being wedged under the piping. The iron rod (15) was clamped on the rod (22) and a wire at its outer end worked the counter. The counter was pulled back by a spring not shown in the picture. The number of revolutions is found by multiplying the reading of (m) by two since the rod (22) moves up and down once in every two revolutions.

For the number of explosions the counter (n) was attached to the valve (1), which supplies gas. When gas was admitted the valve was raised and this worked the counter. The gas for combustion was

measured by the meter (d) and gas
for ignition by the meter (e).

The temperature of the incoming
gas was measured by the ther-
mometer (a) placed in a thermometer
well (b) in the supply pipe.

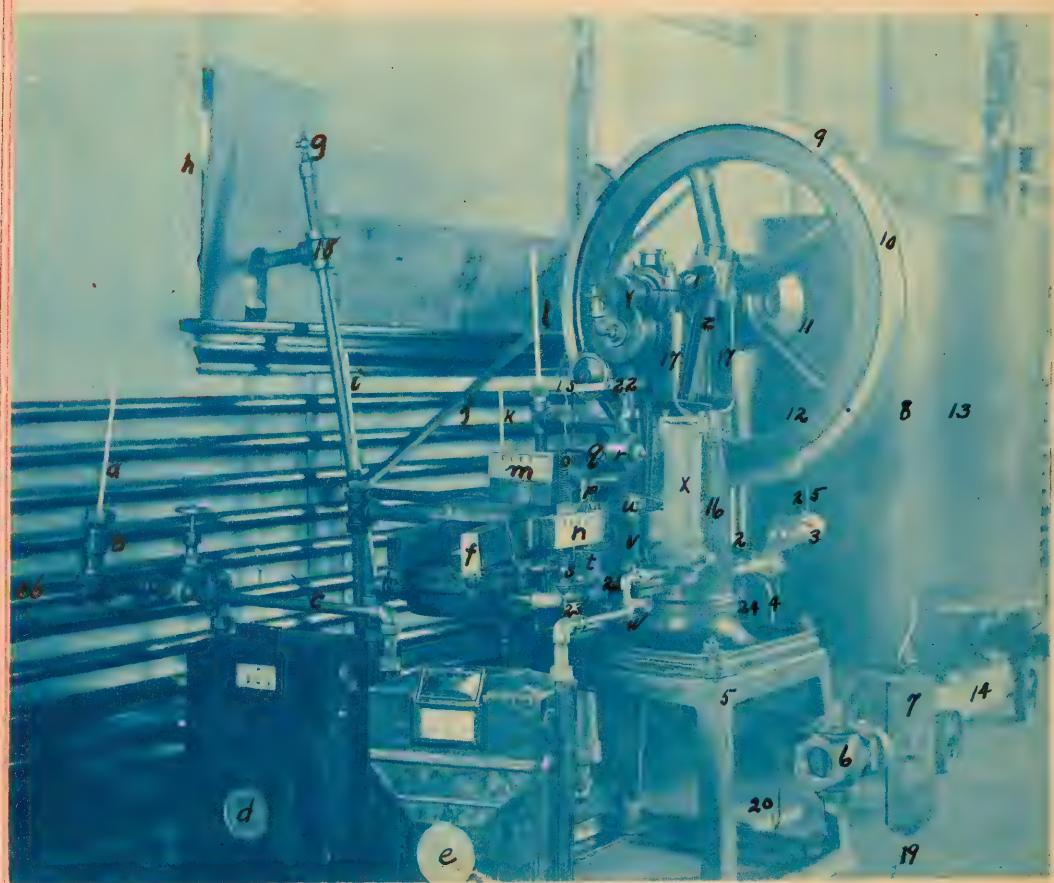
The temperature of the exhaust
gases was determined by the thermom-
eter (i) also in a thermometer well.

A Bristol Recording Gauge - not
shown in picture - in communication
with (26) recorded the gas pressure
in inches of water.

The temperature of the room was
measured by the thermometer (h).
In order to keep the cylinder
cool a certain amount of water,
regulated by the outlet cock was
allowed to flow through the jacket
and was caught in buckets.

and weighed, the buckets being weighed full and empty. Thermometers (K) and (L) placed in thermometer wells on the pipes measure the temperatures of the water at inflow and outflow respectively. The flow was equalised so the rise in temperature of the water was about constant during the test.

The clearance volume was determined by removing the piston and filling the cylinder up to a certain mark with water. The weight of this water was determined by taking the difference in weight of a bucket of water before the water to fill the cylinder was taken out, and after. The difference gives the weight and from this the



volume up to the mark was determined by finding the weight of a known volume of the water in a 200 c.c. bottle. By determining the volume from the mark to the bottom of the piston when at the bottom of its stroke and subtracting this from the first volume gives the clearance volume.

The circumference of the fly wheel was determined directly by wrapping a tape measure around it.

Calibration of Instruments.

The gas meters were calibrated by connecting them in series to the top of a stand pipe filled with water. The water was then run out into a tank



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Calibration of Instruments.

The gas meters were calibrated by connecting them in series to the top of a stand pipe filled with water. The water was then run out into a tank

and weighed and the volume calculated. The water in the meters before and after were taken and from these the readings of the meters for each cubic foot determined.

The indicator spring was calibrated by placing it on a siphon on a steam line and throttling the steam, readings being taken ascending and descending when the pressure was indicated by the steam gauge on the siphon on the steam line. The accuracy of the gauge was then tested with the Grosby Gauge Tester. The spring used was marked 100 lbs. The spring balance was calibrated by hanging standard weights on it and was found correct.

As the 'Kinetol Recording Gauge' read above the atmosphere, one leg of a manometer was opened to the atmosphere and the other connected to a glass tube by means of a rubber tube. One other leg of the Y was connected to the gauge and by blowing into the third leg, any pressure desired above the atmosphere could be measured on the manometer and compared to the gauge. The gauge was found correct. The humidity was found from the report of the U. S. Weather Bureau for Philadelphia.

Definitions.

H_b = barometric height in inches of mercury

P_b = barometric pressure in pounds per square foot $P_b = H_b \times 4888 \times 144$

P_a = press. of air $= P_b - P_{aw}$

P_{aw} = vapor preso. in air, assuming air saturated.

w = % humidity

P'_{aw} = vapor pressure in air at saturated degree of saturation. $P'_{aw} = w P_{aw}$.

w_{aw} = wt. of moisture in 1 cu. ft. of saturated air

w_{aw} = " " " " " air, when humidity is $\frac{w}{100}$. $w_{aw} = w w_{aw}$.

T_a = absolute temp. of air

b_a = percentage of air by weight in mixture of gas and air

b_g = percentage of gas by weight in mixture of gas and air. b_g = air, air weight Gas.

$$V_{\text{air}} = \text{vol. of air} = \frac{V_a}{V_g} Hg$$

V_a = mass of air for explosions

$$V_a = \text{total vol. of air per hour} = \frac{M_a V_a T_a}{P_a}$$

R_a = constant of air

V_a' = vol. of air per hour for explosions.

$$V_a' = \text{vol. of air per minute} = \frac{V_a}{60}$$

$$V_a' = \text{vol. of air per min. for explosion} = \frac{V_a}{60}$$

T_{air} = temp. of air corresponding to, in min.
 P_{air} .

$$M_a = \text{mass of air per explosion} = \frac{V_a}{V_g} Hg$$

Hg = mass of air main in cubic ft. water

P_g = press in lbs. per sq. ft. corresponding to

$$P_g = \frac{62.425}{12} \times Hg$$

P_{gas} = press. of mixture in gas, according

gas saturated at temp. to mixture

T_g = abs. temp. of gas in min.

C_{gas} = constant of mixture in respect of saturated
 gas.

V_g = vol. of gas per min. at saturation.

V_a = vol. of air per min. to mixture

P_g = press. of gas = $P_e + P_g - P_{\text{air}}$

\dot{V}_g = vol. of gas per hour w/o ignition.

\dot{V}_e = vol. of gas per hour for ignition.

\dot{V}_{g0} = vol. of gas per hour without ignition.

R_g = concentration of gas

N_r = revolutions per min.

N_a = no. of possible admissions per min. = $\frac{N_r}{2}$

N_e = no. of explosions per min.

T_e = temp. of exhaust gas.

T_x = temp. of exhaust + other.

v_{ex} = vol. of gas per explosion = $\frac{R_g T_g}{N_e}$

v_{eg} = specific vol. of gas = $\frac{R_g T_g}{P_g}$.

w_{ex} = water gas loss in vol. = $\frac{v_{ex}}{v_{eg}}$

m_{ex} = wt. of moisture in exhaust gas min.

P_e = press. of exhaust gas = $P - P_{env}$

P_{env} = press. of moisture in exhaust gas.

t_1 = wt. of water per min

t_2 = temp. of water entering

t_3 = temp. of water leaving

q = heat of vaporization

- r = heat of vaporization
 c_v = spec. heat at constant volume
 c_p = spec. heat at constant pressure
 H = wt. of air in cylinder in ft.³ gas.
 R_m = constant for vapor of water at low pressures
 Temp. corresponding to pressure
 P
 ρ_{air}
 M_w = mass of water per meter
 L = calorific value of fuel
 a = area of piston
 P = mean effective pressure = $\frac{A}{L}$.
 A = area of card
 C_a = calorific value of fuel oil
 W_1 = wt. on scale side of rope brake
 W_2 = wt. on opposite side
 $W - W_2 = W$ = net pull on rope brake
 \dot{m}_c = heat of combustion per min.
 \dot{H}_{fa} = heat brought in in air per min.
 H_{am} = heat brought in in moist air per min.

H_o = heat lost by cooling gas.

H_m = heat lost in heating jacket.

H_e = heat loss due to wind.

H_{em} = heat in moist. of exhaust gas per min

H_j = heat carried off by jacket water per min

E_i = indicated work in next unit

H_r = heat lost by radiation.

e = mechanical efficiency

E' = hypothetical efficiency

E'' = actual efficiency

$\frac{P}{R}$ & T in cal.

$P \& T$ = press. and temp. in cylinder

$$\text{vol of gas} = \frac{Mg Rg T}{P}$$

$$\text{vol. of air for explosion} = \frac{Ma Ra T}{P}$$

$$\frac{\text{vol. air taken, inc explosion}}{\frac{Mg Rg T}{P} + \frac{Ma Ra T}{P}} = \frac{(Ma - Ma') Ra T}{P}$$

$$Ma' = Ma \frac{1e}{Na} - Mz \cdot \frac{Rg}{Ra} \cdot \frac{Na - Ne}{Na} \quad (1)$$

$$H_c = C_a \times w_{ge} \times Ne \quad (2)$$

$$H_a = c_p \frac{Ma}{60} \times (T_a - T_{32}) \quad (3)$$

$$H_{au} = w_{au} \left[\frac{q_{au}}{w_{au}} + r_{au} + .48(T_a - T_{au}) \right] \frac{1}{r_a} \quad (4)$$

$$H_g = c_p \frac{T_g}{60} (T_g - T_{32}) \quad (5)$$

$$H_{qm} = w_{qm} \left(q_{qm} + \frac{t_{qm}}{60} \right) \frac{V_g}{60} = w_{qm} \times \lambda_{qm} \times \frac{1}{60} \quad (6)$$

$$H_e = c_p \left(\frac{T_e}{60} - \frac{T_{32}}{60} \right) \frac{1}{60} \quad (7)$$

$$H_{ew} = w_{ew} \left[q_{ew} + r_{ew} + .48(T_e - T_{ew}) \right] \quad (8)$$

$$H_f = \frac{Ma}{60} (q_1 - q_2) = Mf (q_1 - q_2) \quad (9)$$

$$H_i = \frac{(I \cdot H \cdot P) \times 33000}{778} \quad (10)$$

$$H_T = (H_c + H_a + H_{au} + H_g + H_{qm}) - (H_e + H_{ew} + H_f + H_i) \quad (11)$$

$$\frac{P_e \Delta}{P_{ew} \Delta} = \frac{Ma Ra T_e}{w_{ew} Ra T_e} \quad . \quad P_e - P_{ew} = P_e$$

$$P_e = \frac{Me Re}{W_{em} R_m} P_{em} = \frac{Me Re}{W_{em} R_m} (P_0 - P_e)$$

$$\left(1 + \frac{Me Re}{W_{em} R_m}\right) P_e = \frac{Me Re}{W_{em} R_m} P_0$$

$$P_{em} = P_e \frac{W_{em} R_m}{Me Re} = P_0 \frac{Me Re}{W_{em} R_m (1 + \frac{Me Re}{W_{em} R_m})} \cdot \frac{W_{em} R_m}{Me Re}$$

$$P_{em} = \frac{P_0}{1 + \frac{Me Re}{W_{em} R_m}} \quad (12)$$

$$W_{em} = 9H \frac{M_g}{68} + W_{air} \dot{V}_a + \dot{V}_{gm} \dot{q}_g \quad (13)$$

$$I.H.P. = \frac{PLa Ne}{33000} \quad (14)$$

$$B.H.P. = \frac{3 \pi r N t W}{33000} \quad (15)$$

$$\text{Vol. of gas per I.H.P. without ignition} = \frac{V_g}{I.H.P.} \quad (16)$$

$$\text{" " " " with " " } = \frac{V_g + V_s}{I.H.P.} \quad (17)$$

$$\text{" " " " B.H.P. without " " } = \frac{V_g}{B.H.P.} \quad (18)$$

$$\text{" " " " with " " } = \frac{V_g + V_s}{B.H.P.} \quad (19)$$

$$e = \frac{B.H.P.}{I.H.P.} \quad (20)$$

$$E' = 1 - \frac{T_3}{T_4} \quad v_3 = \text{clearance vol + vol. of smoke}$$

$$v_4 = \text{clearance vol}$$

$$\frac{T_3}{T_4} = \left(\frac{v_4}{v_3}\right)^{\kappa-1} \quad E' = 1 - \left(\frac{v_4}{v_3}\right)^{\kappa-1} \quad (21)$$

$$E'' = \frac{H_i}{H_c} \quad (22)$$

$$E_2 = \frac{E''}{E'} \quad (23)$$

Tables.

Table 1.

Counters.

Time.	Rev.	Explosion.
12.37	4919	7822
12.43	5920	8072
12.50	7280	9700
12.56	1430	10720
1.01	9770	11072
1.07	10080	10080
2.05	9700	10090
2.31	9470	10840
2.36	10580	11470
2.41	11240	11710
2.46	11800	12700
2.51	11480	13740
2.56	103130	14750

Table 2.

Temperatures.

Time.	Gas. Inlet Exhaust	Jacket Water: Inlet Exhaust	Air.
12.37	84	363	80
12.43	84	387	78
12.50	84	436	79
12.56	84	461	77.5
1.07	84	474	78
1.07	84	479	79
2.25	86	404	80
2.31	86	419	82
2.36	86	420	82
2.41	86	428	77.5
2.46	86	428	81
2.51	86	429	80
2.56	86	426	80.5

Table 3.

Jacket Water.

Time.	No. Bucket	Empty. lbs. oz.	Full. lbs. oz.
12.37.00	1	2 14 $\frac{1}{4}$	22 15 $\frac{1}{2}$
12.41.10	2	2 11 $\frac{3}{4}$	20 15 $\frac{1}{2}$
12.45.00	1	2 14 $\frac{1}{2}$	21 4
12.50.00	2	2 11 $\frac{1}{2}$	23 13 $\frac{1}{4}$
12.54.10	1	2 14 $\frac{1}{2}$	21 11 $\frac{1}{2}$
12.58.30	2	2 11 $\frac{1}{2}$	21 00 $\frac{5}{4}$
1.04.00	1	2 14	12 11
1.07.00	-		
2.25.00	1	2 14 $\frac{3}{4}$	20 a $\frac{1}{4}$
2.29.45	2	2 11 $\frac{3}{4}$, a1	14 $\frac{1}{2}$
2.35.10	1	2 14 $\frac{1}{2}$	22 15 $\frac{1}{2}$
2.38.40	2	2 11 $\frac{1}{4}$	22 13 $\frac{3}{4}$
2.46.35	1	2 14 $\frac{3}{8}$	22 8 $\frac{1}{4}$
2.47.30	2	2 11 $\frac{3}{8}$	24 2
2.52.00	1	2 14 $\frac{1}{2}$	22 3 $\frac{1}{2}$
2.56.10			

Table 4.

Meters - Gas.

Time	Cylinder	Time.	Ignition.
12.26.35	0	12.37.45	0
12.31.50	2	12.48.30	1
12.36.45	4	1.00.00	2
12.41.55	6	1.06.15	2.5
12.47.25	8	—	—
12.53.00	10	—	—
12.57.50	12	—	—
1.00.05	13	—	—
2.26.35	0	2.18.30	0
2.32.00	2	2.29.30	1
2.37.10	4	2.52.30	3.
2.42.25	6	—	—
2.47.30	8	—	—
2.52.30	10	—	—
2.57.20	12	—	—

Table 5.

Brake.

Time.	lbs.	oz.
16.57	2	15
16.43.	3	6
16.30	3	4
16.36.	3	8
1.07	3	10
1.07.	3	10
2.05	3	8
2.31	3	8
2.36.	3	10
2.41	3	10
2.36.	3	10
2.31.	4	0
2.36.	4	0

Wt of poise - 14 $\frac{1}{2}$ oz.

" " balance - 2 lbs. 3 $\frac{1}{4}$ oz.

Additional Readings.

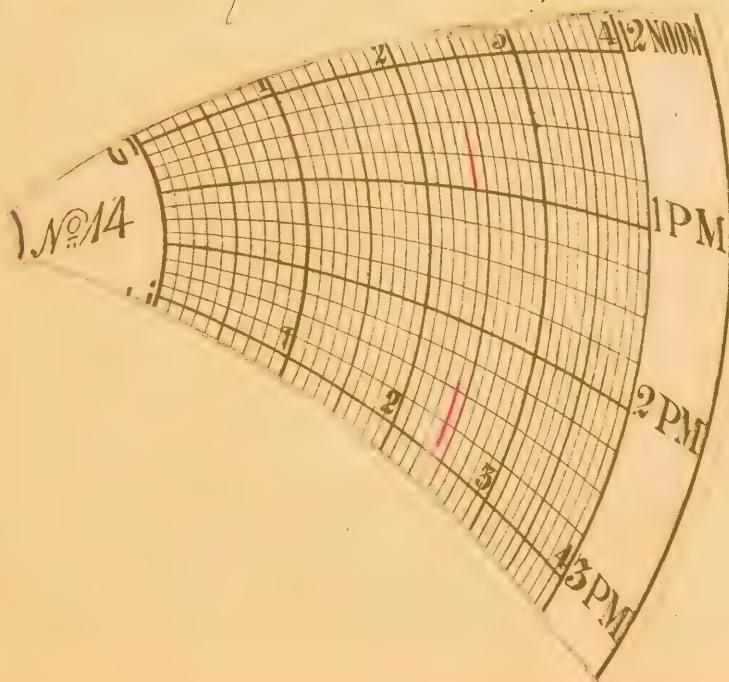
Calibration of Miles.

Cylinder meter 1 cu. ft 1.177 cu. ft.
 Liquid water 1 cu. ft. .001 cu. ft.

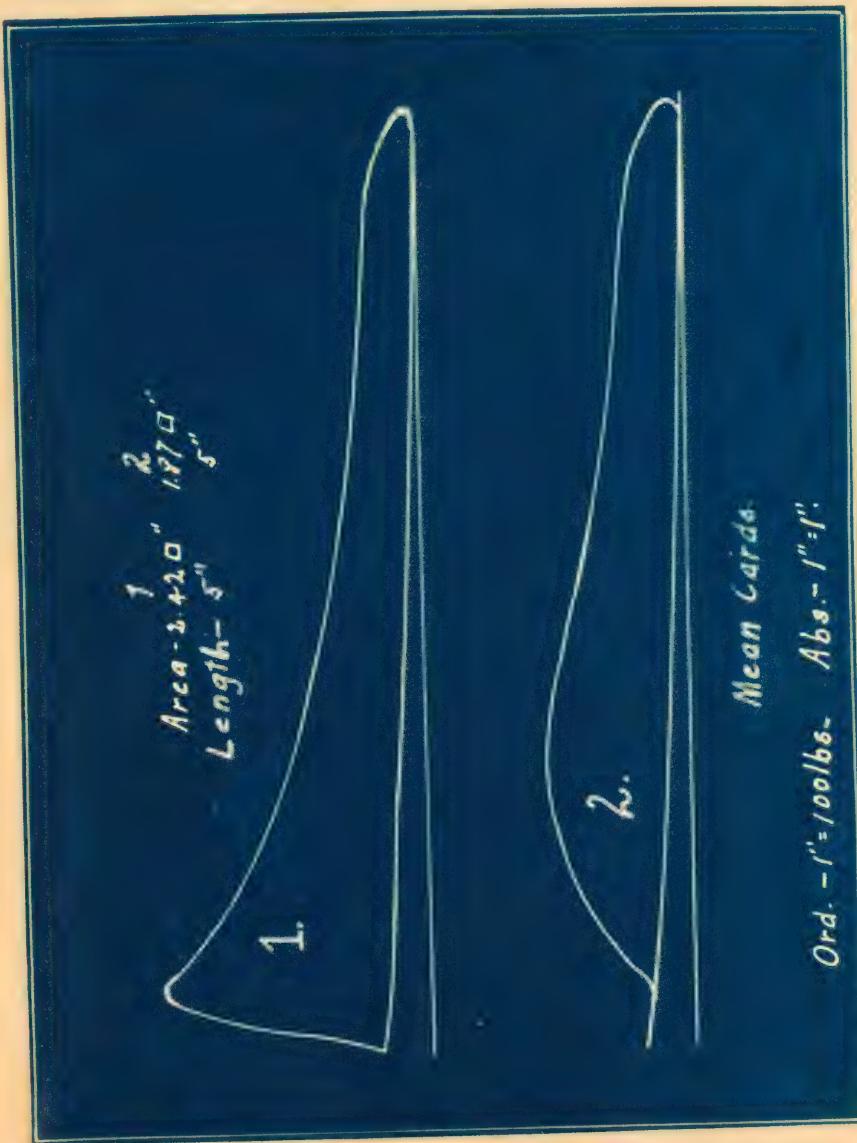
U. S. WEATHER BUREAU, Philadelphia,
 Monday, May 1, 1899.

Time...	Barometer...	Wind.				Rainfall.....	State of Weather....
		Relative Humidity...	Tem- perature...	Direc- tion...	Veloc- ity...		
8 A. M.	30.11	61	83	S. W.	12	0	Pt. Cl'dy
8 P. M.	30.00	74	59	S. W.	12	0	Pt. Cl'dy

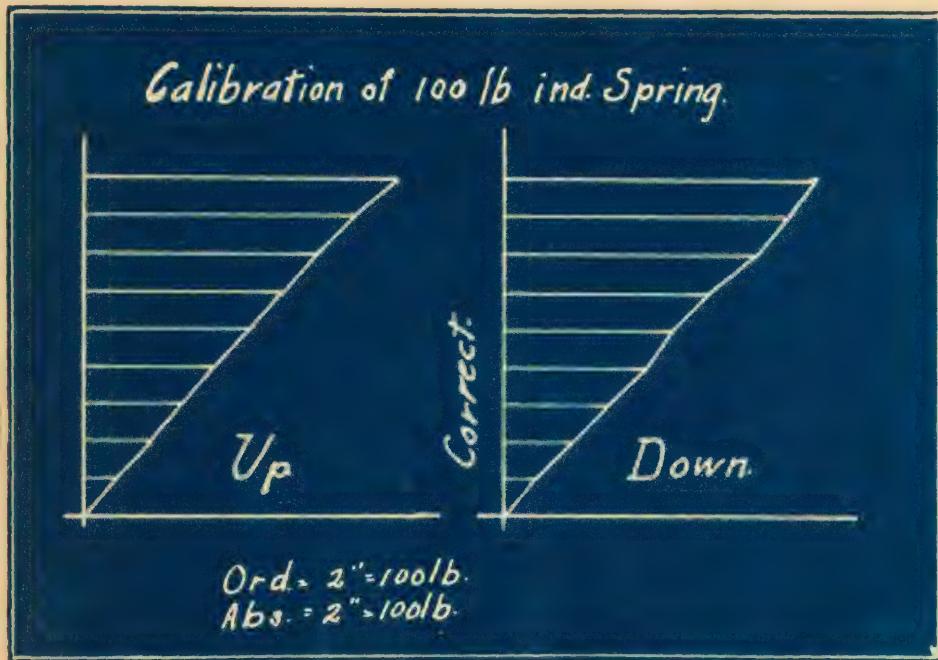
Bristol Recording Gauge
 Card from Gas Main:



Mean Cards.



Indicator Spring Calibration Curve.



The Mean Cards above were constructed in the following manner: Each card had its base divided into 10 parts: In order for these parts to be equal parts of the stroke, the angularity,

of the connecting rod and string
was allowed for by connecting
up the indicator as in use and
moving the piston equal parts
of its stroke and a mark
made with the indicator pencil
on a paper on the drum and
the cards correspondingly marked.
The distances on the mean card
were made equal and the
corresponding pressures corrected
according to the spring cali-
bration.

Test.

In starting the test the engine was run up to speed with the required load and run for about a quarter of an hour under the conditions of the test until the temperatures become steady. The test was started by a simultaneous reading of the revolution and explosion counters. Then the temperatures of the room, inlet and exhaust gases, and inlet and discharge jacket water and the reading of the brake were made in order and a card taken from the indicator. This series of operations was repeated every five minutes. One min

ute before the beginning of the test a bucket was placed under the jacket water outlet and as the buckets filled they were weighed and emptied. Two buckets were used and one minute before the end of the test the last bucket was removed and weighed, the water flowing at practically the same rate all the way through. The test was ended by taking a simultaneous reading of the revolution and explosion counters after which the temperatures and brake were read to fill out the readings, before the engine was stopped at intervals during the

Test samples of the fresh and exhaust gases were taken and were subsequently analyzed in a set of Tempel's apparatus.

The exhaust gas was drawn from the pipe (18) by a rubber tube attached above the cock (9) and the gas collected over water in a sealed bottle. By opening the cock (9) the gas was drawn out.

A similar arrangement on the gas main (26), not shown in the picture, allowed the fresh gas to be collected.

The time the two cubic foot hand of the combustion gas meter passed a mark just before the test, was noted and every time it again passed the mark was noted until after the end of the

test. From this the gas and Henry
The test was computed.

In a similar manner many
time the equation water hand
placed a cubic root mark.
The time was noted.

Results.

Analyses of Gases.

Philadelphia Illuminating Gas.

	% Vol.		% Wt.
CO_2 -	2.4	$\times 22 = 52.7$	6.70
CO -	16.5	$\times 14 = 230.5$	29.30
C -	.6	$\times 12 = 7.2$	1.22
C_2H_4 -	5.2	$\times 14 = 72.8$	9.89
H -	31.7	$\times 1 = 31.7$	4.05
C_3H_8 -	37.1	$\times 8 = 296.5$	37.65
N -	$\frac{6.5}{100.0}$	$\times \frac{14}{78.21} = \frac{88.1}{782.1}$	$\frac{11.19}{100.0}$

Exhaust Gas

	% Vol.		% Wt.
CO -	0	$\times 14 = 0$	0
CO_2 -	7.00	$\times 22 = 15.4$	0.56
O -	5.45	$\times 16 = 87.2$	6.49
N -	$\frac{17.00}{100.0}$	$\times \frac{14}{146.3} = \frac{121.0}{146.3}$	$\frac{82.95}{100.0}$

Properties of Gases

Philadelphia Illuminating Gas

	C_P	C_V
CO_2	$6.7 + .217 = 1.453$	$6.7 \times 1.1535 = 1.03$
CO	$29.3 \times .2479 = 7.260$	$29.3 \times 1.1758 = 5.15$
O	$1.22 \times .2175 = .265$	$1.22 \times 1.1535 = .189$
H	$4.05 \times 3.409 = 13.800$	$4.05 \times 2.412 = 9.750$
CH_4	$37.65 \times .593 = 22.350$	$37.65 \times .467 = 17.35$
C_2H_4	$9.89 \times .404 = 3.990$	$9.89 \times 1.352 = 3.28$
N	$11.19 \times .2438 = \frac{2.730}{51.848}$	$11.19 \times 1.173 - \frac{1.955}{38.864}$

$$R_g (1.06 \text{ gas}) = .51848 - .38864 = .12984 \text{ B.T.U.} \\ = 101.2 \text{ foot pounds.}$$

Exhaust Gas

C_p	C_v
$CO_2 - 10.36 \times .217 = 2.285$	$10.36 \times .1335 = 1.621$
$O_2 - 0.49 \times .2175 = 1.410$	$0.49 \times .13 = 0.636$
$N_2 - 82.95 \times .2438 = \frac{20.250}{23.945}$	$82.95 \times .173 = \frac{14.350}{16.977}$

$$R_e \text{ (per lb of gas)} = 23.945 - 16.977 = .06968 \text{ B.T.U.} \\ = 54.211 \text{ foot-lbs.}$$

Gas for ignition in cubic ft per hour. Found by dividing the number of cu. ft by the time in minutes taken to pass through, multiply by 60 and divide by calibration of the meter.

$$\text{Gas-ignition} = \frac{5.5 \times 60}{62.5 \times 1.001} = 5.28 \text{ cu ft}$$

Same for gas for combustion

$$\text{Gas} \quad \frac{25 \times 60}{64.15 \times 1.177} = 19.8 \text{ cu. ft. per hour}$$

Calorific Value of Gas.

$$\text{CO} — 4300 \times .293 = 1259.$$

$$\text{CH}_4 — 23500 \times .3765 = 8847.75$$

$$\text{C}_2\text{H}_4 — 21400 \times .0989 = 2116.46$$

$$\text{H} — 52500 \times .0405 = \underline{\underline{2126.25}}$$

Value per lb. gas = 14349.46 B.T.U.

Ratio of air to gas by weight.

Find the ratio of gas to carbon in the fresh gas and multiply by the per cent of carbon in octane fuel. The result is the per cent of gas supplied to form the exhaust gas. The remainder of exhaust gas is air.

11

gas in combustion of gas and air.

$$\begin{aligned}
 \text{fresh gas} &= \% \text{ C} \\
 \text{C in } \text{CO}_2 &= \frac{1}{2} \times 6.7 = 3.35 \\
 \text{C in } \text{CO} &= 12.57 \\
 \text{C in } \text{C}_2\text{H}_4 &= \frac{24}{2} \times 7.19 = 8.48 \\
 \text{C in } \text{C}_6\text{H}_6 &= \frac{12}{6} \times 37.6 = \underline{\underline{28.23}} \\
 \text{Total C} &= 51.13
 \end{aligned}$$

Exhaust gas % C

$$\text{C in } \text{CO}_2 = \frac{2}{4} \times 3.35 = 2.88 \quad \text{Total C}$$

$$\% \text{ Gas} = \frac{100}{51.13} \times 2.88 = 5.64\%$$

% air supplied = $100 - 14.6$

$$\begin{aligned}
 \therefore \text{Lbs of air per lb of gas} &= \frac{94.36}{5.64} \\
 &= 16.75 \text{ lbs}
 \end{aligned}$$

Specific Volume of gas in
main = $\frac{RT}{P}$

P bar. atm. + gauge pres. - vapor pres.

$$\text{Bar. pres.} = 30.06 \times 4.888 = 14.69 \text{ lbs per sq. in}$$

$$\text{Gauge pres.} = 2.4 \times 0.361 = .0866 \text{ lbs per sq. in.}$$

Assume gas is saturated.

Vapor pressure saturated at 85°F.

$$= .391 \text{ lbs per cu. in}$$

$$\therefore P = 14.69 + .0866 - .391 = 14.3856 \text{ lbs per sq. in}$$

$$\therefore \text{Specific Vol} = \frac{101.2 \times (460.7 + 85)}{14.3856 \times 144}$$

$$= 26.9 \text{ cu ft}$$

$$\text{Vol. gas per explosion} = \frac{\text{cu. ft. per boom}}{60 \times \text{explos. per min.}}$$

$$= \frac{19.8}{60 \times 141.1} = 0.0233876 \text{ cu ft}$$

Weight of gas per explosion

$$\text{vol. per explosion} \cdot \frac{0.0233876}{\text{specific volume}} = \frac{26.98}{26.98}$$

$$= .000056685 \text{ lbs}$$

Wt. of air per explosion = wt. of gas per
explosive x ratio air to gas = 16.73×0.0008665
= .00145197 lbs.

Total air per hour = $.00145197 \times 14.1 \times 60$
= 12.2915 lbs.

Volume of air per hour = $\frac{MRT}{P}$

P = Bar. Pres - vapor pressure

T = 86.23 Saturation = 71%

Bar pressure = 14.72 lbs per sq. in.

Pressure assuming saturation = .61 lbs

∴ vapor pressure = $.61 \times .71 = .43$ lbs per sq. in.

$$\therefore P = 14.72 - .43 = 14.29$$

$$\therefore V = \frac{14.29 \times 14.71 \times (86.23 + 160.7)}{14.29 \times 144}$$

$$= 174.375 \text{ cu. ft. per hour}$$

Volume of air used only when
explosions. When there
are explosions, only air is

drawn in. Assuming the pressure on gas and air is same and that cylinder volume is sum of the volumes of the gas and air we get formula (1). *

$$M_a' = 12.29 \times \frac{141.1}{\frac{318.4}{2}} - \frac{18.1 \times 101.2 \times 0.00086685 \times 141.1 \times 60}{\frac{318.4}{2}} = 10.893 - 15.821 = 10.735 \text{ lbs per hr}$$

$$\therefore \text{Lbs per explosion} = \frac{10.735}{60 \times 141.1} = .001268 \text{ lbs}$$

$$\begin{aligned} &\text{Volume of air for explosions per hour} \\ &= \text{total vol of air} \times \frac{\text{wt. air for explosion}}{\text{wt. of total air}} \\ &= 174.375 \times \frac{10.735}{12.29} = 152.31 \text{ cu ft.} \end{aligned}$$

$$\begin{aligned} &\text{Volume per explosion} = \frac{152.31}{60 \times 141.1} \\ &= .017991 \text{ cu. ft.} \end{aligned}$$



Indicated P. - See formula (14).
P was found from the cards.
 Since there were 5 cards like the first and 7 like the second, they were multiplied by these numbers respectively and divided by the sum to find mean and then by the factor for m.h.p.

$$I. \underline{P} = \frac{41.98 \times 5 + 7 \times 1.87}{12 \times 5} = 41.98$$

$$= .527$$

$$\text{since } M. + P. = \frac{12.42 + 7 \times 1.87}{12 \times 5}, \text{ mean} = 41.98$$

Brake Horse Power - See formula (15)
W is found by adding the weight of the spring balance in the indicated pul and subtracting the weight on the other end.

$$B.P = \frac{318.4 \times 6.28 \times 4.87}{33000} = .295$$

Gas per I.P. without ignition per hour = $\frac{19.8}{.295} = 67.11$ cu ft

$$\begin{aligned} \text{Same with ignition gas} &= \frac{19.8 + 5.28}{.295} \\ &= 47.39 \text{ cu. ft.} \end{aligned}$$

Gas per B.P. per hour without ignition
= $\frac{19.8}{.295} = 67.11$ cu ft.

$$\begin{aligned} \text{Same with ignition gas} &= \frac{25.08}{.295} \\ &= 85.02 \text{ cu. ft.} \end{aligned}$$

Cleanance.

wt. of water in cylinder = 2.919 lbs.

wt. of 15.23 cu. in. of water = .547 lbs.

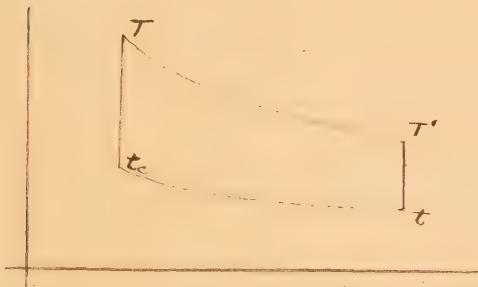
vol. vol. of water = $\frac{2.919 \times 15.23}{.547 \times 1728} = .047 \text{ cu. ft.}$

vol. of displacement = $\frac{32 \times 7.0524 \times 8\frac{1}{3}}{1728} = .3362 \text{ cu. ft.}$

then $T_c = 147^\circ \text{R} \approx 0.08 \text{ ad. ft}$

Efficiencies.

$$e = \frac{295}{527} = .56 \quad \text{from formula (20)}$$
$$E'' = \frac{.527 \times 330000}{778 \times 1.2739 \times 147.1} = .1274 \quad \text{formula (24)}$$



$$E' = \frac{c_o(T-t_c) - c_v(T'-t)}{c_o(T-t_c)}$$

Since both curves are adiabatic, and pass through the same volume change

$$\frac{T'}{T} = \frac{t}{t_c}$$

From this we have $\frac{T'-t}{T-t_c} = \frac{T'}{T} = \frac{t}{t_c}$. Then
 $E' = 1 - \frac{T'}{T} = 1 - \frac{t}{t_c}$.

In para 24, formula 24, E' is expressed in terms of t , in adiabatic terms it becomes

the temperatures by their equivalents in volumes.

$$\text{Volume of piston displacement} = \frac{\pi^2 \times 28.4 \times 5}{1728} \\ = .0204 \text{ cu. ft.} = 0.7$$

$$\text{Total volume} = .0204 + .0108 = .0312 = 0.3$$

$$E' = 1 - \left(\frac{.0108}{.0312} \right)^{1/4} = 1 - .647 = .353$$

$$E_2 = \frac{.1274}{.353} = .361 \quad \text{formula (23).}$$

Heat Entering Engine.

$$H_C = 14349.46 \times .000086685 \times 141.1 = 175.87 \text{ B.T.U.}$$

per min. formula (23)

$$H_a = .2375 \times 16.75 \times .000086685 \times 141.1 \times (86.23 - 32) \\ = 2.6387 \text{ B.T.U. per min. formula (3).}$$

Heating in air.

wt. of vapor in cu. ft. of saturated air at 86.23°

$$F = w_{av} = .001914 \text{ lbs.}$$

$$\text{wt. of air humidity} = 71\% \text{ or } h_{av} = w_{av} \\ = .71 \times .001914 = .001359 \text{ lbs.}$$

Vapor press. at 86.23 when saturated = $P_{am} =$
 610.7 mm. Hg

P'_{am} = press at 77% humidity = $.77 \times 610.7 = 437.757 \text{ mm. Hg}$

T_{am} = corresponding temp. to $P'_{am} = 75.63$.

When the air is not saturated, the vapor is superheated, and therefore the heat brought in in the moisture is equal to the heat of the liquid, the heat of vaporization and the latent superheat. By formula (4)

$$H_{am} = .001354 [43.75 + 1061.3 + .48(86.23 - 75.63)]$$
$$\times \frac{174.375}{60} = 4.3844 \text{ B.T.U. per min.}$$

$$H_g = .5785 \times .000086685 \times 141.1 \times (85 - 32) =$$
$$= .33612 \text{ B.T.U. per min. formula (5)}$$

Since the fresh gas is saturated with moisture, the heat brought in in the moisture is equal to the heat of the liquid and the heat of vaporization. by formula (6)

$$H_{qm} = .001813 \times 1107.9 \times \frac{19.8}{60} = .66284$$

.001813 lbs. is the mass of moisture in 1 cu. ft. of gas at the temperature of the gas 85°F . when saturated.

Heat leaving Engine.

The indicated work is here expressed in B.T.U. by formula (10)

$$H_i = \frac{5274 \times 33000}{478} = 22.353 \text{ B.T.U. per min.}$$

The heat leaving in the jacket water, as expressed by formula (9) is the mass of water multiplied by the difference between the heat of the liquid at entrance and exit.

$$H_j = \frac{261.75}{60} \times 26.1 = 113.861 \text{ B.T.U.}$$

$$H_e = .23445 \times (427.4 - 32)(.20486 + .01223) \\ = 20.554 \text{ B.T.U. By formula (7)}$$

Water-vap. pressure = .00.

$$H \text{ in } 1\text{ lb. fresh gas (free)} = .0405 \text{ lb.}$$

$$H \text{ in } C_2 H_4 = \frac{4}{28} \times .0989 = .0141 \text{ "}$$

$$H \text{ in } C H_4 = \frac{4}{16} \times .3765 = .0941 \text{ "}$$

$$\text{Total } H \text{ in } 1\text{ lb. of gas} = .1487 \text{ "}$$

$$\text{wt. of } H_2 O \text{ formed from } H = 4 \times .1487 = 1.3383 \text{ lb.}$$

$$\text{amt. of gas per min.} = .01223 \text{ lbs.}$$

$$H_2 O \text{ formed per min.} = .01223 \times 1.3383 = .01637 \text{ lbs.}$$

$$H_2 O \text{ in air per min.} = .00395 \text{ "}$$

$$\text{" " gas " "} = \underline{.00060 \text{ "}}$$

$$\text{Total moisture} = .02092 \text{ "}$$

By formula (12) we obtain pressure
of vapor, and from tables the cor-
responding temperature must be
found.

$$P_{\text{vap}} = \frac{14.72}{1 + \frac{.21704 \times 54.211}{.02092 \times 85.732}} = 1.95 \text{ lbs. "}$$

$$\text{Corresponding temp.} = 125.16$$

From a similar formula to that used in finding heat given off in combustion of air we have by formula (8)

$$\text{Heat} = .02092 [93.5 + 1026.7 + 48(427.4 - 125.4)] \\ = 26.466 \text{ B.T.U.}$$

Heat Produced.
Combustion

	per min.	per 100 B.T.U.
Combustion	175.57000	95.629
Air	2.63870	1.438
Moist. of Air	14.38440	2.389
Gas	.33612	.183
Moist. of Gas	<u>.66284</u>	<u>.361</u>
	183.53206	100.000

Savings.

	per min	per m. B.T.U.
I.H.P.	22.353	12.174
Ex. Water	113.461	02.038
Ex. Gas.	20.534	11.200
Oil & Lub. Gas	26.466	1.430
Lubrication	<u>.299</u>	<u>.163</u>
	183.532	100.000

The next item in calculation is
the amount of heat by which
the heat leaving the engine
is less than the heat entering.
 $\therefore = 183.532 - 183.233 = .299 \text{ B.T.U.}$

Result of test

Day 1 10.10 A.M.

1.	Operation of valve in minutes	60
2.	Diameter of cylinder in inches	3
3.	Length of stroke in inches	5
4.	Circumference of flywheel in feet	6.28
5.	Atmospheric pressure (barometer) 30.36	
6.	" " lbs. per cu. in.	14.69
7.	Pressure in gas main in inches water	2.4
8.	Max. pressure in cylinder above atmosphere here in lbs. per cu. in.	114
9.	Mean effective pressure in lbs per cu. in.	41.98
10.	Clean temperature of air	86.23
11.	" " " fresh gas	85
12.	" " " exhaust air	40.74
13.	" " " entering water	80.2
14.	" " " leaving "	88.4
15.	" effective pull on brake in lbs.	4.81
16.	Revolutions per minute	318.4
17.	Explosions per minute	141.1

18.	Dredged horse power	.527
19.	Brake horse power	.295
20.	Gas per hour without ignition (cu. ft.)	19.8
21.	" " " for " (")	5.28
22.	Total gas per hour (cu. ft.)	25.08
23.	Wt. of gas per explosion (lb.)	.000286681
24.	Vol. of gas per explosion (cu. ft.)	.002333876
25a	Calorific value of gas per lb. in B.T.U.	14349.5
25.	" " " per explosion "	1.2489
26.	Gas per B.H.P. per hr. without ignition (cu. ft.)	37.57
27.	" " " with " (")	47.69
28.	" B.H.P. " without " (")	67.11
29.	" " " with " (")	85.06
30.	Wt. & air per lb. of gas	16.75
31.	wt. of air per explosion (lb.)	.00145797
32.	vol. of air per explosion (cu. ft.)	.017991
33.	vol. of air per hr. for explosion (cu. ft.)	152.31
34.	Total air per hour (cu. ft.)	174.375
35.	Total air per hour (lbs.)	122915
36.	use efficiency	.75

37.	Actual efficiency	.1277
38.	Mechanical work type	361
39.	Mechanical efficiency	.06



*Equation of
Curvature
is*

*The general
equation of the
curve is*

$\frac{dy^m}{dx} = k$
~~by the method
of least squares~~
~~the value of the
coefficient k~~
~~may be obtained~~
~~the equation~~
 $k = m \cdot l$ is
 expressed in
 the following
 form -
 $y = mx + c$

equivalent point was selected
on the abscissa and the pressure
and volume for each point meas-
ured on the curve. The logarithms
of these values were substituted
in the equations given above.

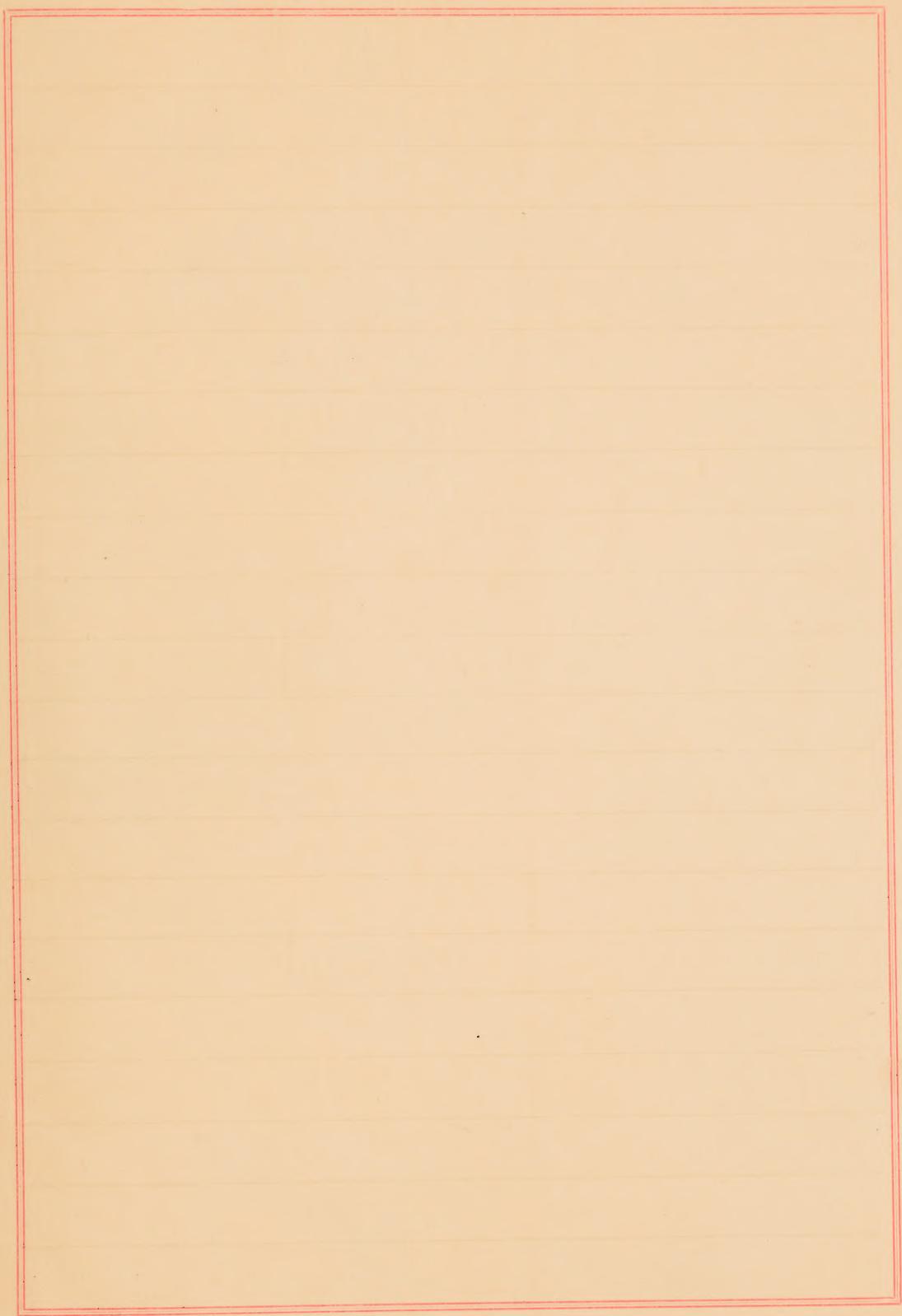
Then the coefficient of ν was
taken and used as a multiplier
in each equation. This a second
set of equations were obtained.
Each set were added and
two equations containing
two unknowns - K and ν -
were obtained. These were solved
for ν .

Then the above work was
drawn. According to the value
of ν the expansion curve
should fall above or below
the curve $Pv = K$. If ν is less

than one the expansion curve should fall above $p_0 = K$. If greater than one the curve $p_{v_n} = K$ should fall below the curve $p_0 = K$.

Solving for n as described above we obtained a value

$$n = 1.154.$$



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N/1198/03073/4029X

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